Review article

Mixing and formulation of low dose drugs: underlying problems and solutions

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Abstract:

Mixing and formulation of low dose drugs can be very challenging due to problems related to segregation, content uniformity and physical stability. A careful control on these factors is necessary while manufacturing low dose drug products. Selection of excipients for the specific steps during formulation/process development is critical to develop a homogenous and segregation-free low dose formulation. Many types of equipments have been designed to facilitate mixing of low dose drugs with excipients. Apart from conventional formulation techniques (like wet granulation, dry granulation, and direct compression) various new techniques have been reported such as high shear granulation, ordered mixing and spray drying. These technological advancements have improved the manufacturing and quality of low dose drug products by achieving their predefined objective of content uniformity during mixing and formulation of low dose drugs. This article reviews current advancements related to formulation techniques of low dose drugs.

Keywords: Content uniformity; Homogeneity; Low dose drugs; Segregation

Introduction

Progress in pharmaceutical research has produced very potent drugs, which require careful formulation and production in order to produce solid oral dosage forms with acceptable homogeneity and physical stability. Assuring the physical stability of a powder blend for production of tablets or capsules represents a major quality assurance consideration. The content uniformity quality control procedure for most tablets and capsules which are the subject of official monograph is by the analysis of mean drug content of 20 tablets which have been ground together. Table 1 presents low dose drugs for which content uniformity test is mandatory in Indian Pharmacopoeia 1996 edition [1]. Train (1960) realized that such an assay procedure could provide a satisfactory mean value, even though individual tablets showed large variations about the mean. The B.P. recognized the importance of the problem in 1973 and introduced a requirement of individual tablet assay for "micro dose" preparations (tablets containing less than 2 mg or 2% w/w of active drug) [2]. In addition to specific problems

associated with interpretation of the data, in such assays there are also more general problems such as inability to detect batches where loss of homogeneity has occurred up until the testing provides no information concerning the point of failure nor the mechanism by which content uniformity has been lost [3]. In order to solve both specific and general problems associated with current pharmacopoeial testing, simple reproducible and informative tests are required on powder mixes prior to processing.

Latest pharmacopoeial guidelines ensure the consistency of dosage units by uniformity of dosage unit tests. The term "uniformity of dosage unit" is defined as the degree of uniformity in the amount of the active substance among dosage units. The uniformity of dosage units can be demonstrated by either content uniformity or mass variation. The content uniformity method may be applied in all cases. However the test for mass variation is applicable for selected dosage forms as given in Table 2 [4-6].

 Table 1
 List of low dose drugs for oral delivery [1]

No.	Drug	Dose	Category
1	Alprazolam	250 to 500 μ g three times daily	Anxiolytic
2	Amiloride hydrochloride	Initially, 5 to 10 mg daily; maximum 20 mg daily	Diuretic
3	Astemizole	For adults, 10 mg (not to be exceeded) once daily up to 7 days.	Antihistaminic
		For children, 5 mg (not to be exceeded) once daily up to 7 days.	
4	Atropine methonitrate	200 to 600 µg	Anticholinergic
5	Atropine sulphate	250 μg to 2 mg daily in single or divided doses	Anticholinergic; antidote to
			cholinesterase inhibitors
6	Benzhexol hydrochloride	1 mg, gradually increased to a usual maintenance dose of 5 to	Antiparkinson
		15 mg daily in 3 to 4 divided doses	
7	Betamethasone	0.5 to 5 mg daily, in divided doses	Adrenocortical steroid
8	Bromhexine hydrochloride	8 to 16 mg three to four times daily	Expectorant
9	Bromocriptine mesylate	Equivalent of 2.5 mg to 20 mg of bromocriptine daily, in divided	Dopamine agonist
		doses	
10	Buprenorphine hydrochloride	Equivalent of up to 400 μg of buprenorphine every 6 to 8 hours	Narcotic analgesic
11	Busulphan	2 to 4 mg daily; maintenance dose, 0.5 to 2 mg daily	Cytotoxic
12	Carbimazole	Controlling dose, 30 to 60 mg daily, in divided doses; maintenance	Antithyroid
		maintenance dose, 5 to 20 mg daily	
13	Chlorpheniramine maleate	4 to 16 mg daily, in divided doses	Antihistamine
14	Clonidine hydrochloride	50 to 100 μg thrice daily increased gradually according to the	Antihypertensive
		needs and response of the patient; maximum daily dose 1.2 mg	
15	Colchicine	Initial dose, 1 mg; subsequent doses, 500 μg every two hours	Gout suppressant

Table 1 List of low dose drugs for oral delivery [1] (Cont.)

No.	Drug	Dose	Category
16	Cyproheptadine	4 to 20 mg daily, in divided doses	Histamine H1-receptor
	hydrochloride		antagonist
17	Dexamethasone	500 μg to 10 mg daily, in divided doses	Adrenocortical steroid
			(anti-inflammatory)
18	Diazepam	In anxiety states, 2 mg thrice daily, in insomnia associated with	Anxiolytic; sedative;
		anxiety, 5 to 15 mg at bedtime	anticonvulsant
19	Dienoestrol	500 μg to 5 mg daily	Oestrogen
20	Digitoxin	50 to 200 µg daily	Cardiac glycoside
21	Digoxin	62.5 μg to 1.5 mg in divided doses	Cardiac glycoside
22	Dydrogesterone	10 mg twice daily	Progestogen
23	Ergometrine maleate	250 μg to 1 mg	Uterine stimulant
24	Ergotamine tartrate	1 mg to 2 mg	Sympatholytic; antimigraine
25	Ethinyloestradiol	For menopausal symptoms, 10 to 20 μg daily continuously or for	Oestrogen. (For menopausal
		21 days, repeated after 7 days, with a progestogen from day 17	symptoms and primary
		to day 26 of cycle if uterus is intact. For primary amenorrhoea,	amenorrhoea)
		10 μg on alternate days increasing to a maximum of 50 mg daily	
		continuously with a progestogen for the last 5 days of month	
26	Fludrocortisone acetate	50 to 300 µg daily	Mineralocorticoid
27	Fluphenazine hydrochloride	1 to 10 mg daily	Antipsychotic
28	Glibenclamide	5 mg daily, adjusted according to response; maximum 15 mg	Hypoglycaemic
		daily, after food	
29	Haloperidol	1.5 to 20 mg daily	Antipsychotic
30	Melphalan	2 to 4 mg daily for 4 to 6 days	Cytotoxic
31	Methadone hydrochloride	5 to 10 mg every 6 to 8 hours	Narcotic analgesic
32	Methylergometrine maleate	250 μg to 500 μg	Uterine stimulant
33	Nicoumalone	Initial dose, first day, 8 to 12 mg; second day, 4 to 8 mg;	Anticoagulant
		maintenance dose, 1 to 8 mg daily	
34	Nitrazepam	5 to 10 mg daily, at bed time	Hypnotic; sedative
35	Norethisterone	5 to 20 mg daily, in single or divided doses	Progestogen
36	Norgestrel	150 to 300 μg	Progestogen
37	Prednisone	5 to 60 mg daily, in divided doses	Adrenocortical steroid
38	Prednisolone	5 to 30 mg daily, in divided doses	Adrenocortical steroid
39	Prazosin hydrochloride	500 μ g to 1 mg two to three times daily	Antihypertensive
40	Salbutamol	6 to 16 mg daily, in divided doses	Beta-adrenoceptor agonist
41	Thyroxine sodium	50 to 300 μg daily	Inyromimetics
42	l'imolol maleate	In hypertension, initially 5 mg twice daily or 10 mg once daily;	Beta-adrenoceptor
		maximum 60 mg daily. In angina, initially 5 mg 2 to 3 times daily;	antagonist
		maintenance dose, 15 to 45 mg daily. For prophylaxis after	
		infarction, initially 5 mg twice daily, started 1 to 4 weeks after	
10	T (1997)	Intarction. For migraine prophylaxis, 10 to 20 mg daily	
43	Iriamcinolone	2 to 24 mg daily	Corticosteroid

			Dose and	ratio of active
Dosage forms	Types	Subtypes	sub	ostance
			≥ 25 mg	< 25 mg
			and \ge 25%	and < 25%
Tablets	Uncoated		MV	CU
	Coated	Film-coated	MV	CU
		Others	CU	CU
Capsules	Hard		MV	CU
	Soft	Suspension, emulsion, gels	CU	CU
		Solutions	MV	MV
Solids in single-dose	Single component		MV	MV
containers	Multiple components	Solution freeze-dried in final container	MV	MV
		Others	CU	CU
Solutions enclosed in			MV	MV
single-dose containers				
Others			CU	CU

Table 2 Application of content uniformity (CU) and mass variation (MV) test for dosage forms [4-6]

The recommendation given by product quality research institute (PQRI) regarding blend uniformity was reviewed and finally accepted by US FDA. According to this recommendation, sampling plans for process validation batches include identification of at least 10 locations in the blender to pull blend samples and identification of at least 20 locations throughout the compression or filling operation to obtain dosage units. Blend sample criteria includes relative standard deviation (RSD) \leq 5.0% and all individuals should be within the mean ± 10% (absolute). Dosage unit criteria includes RSD of all individuals \leq 6.0%. Each location mean should be within 90.0-110.0% of target potency, and all individuals should be within 75.0-125.0% of target potency [7]. Three factors can directly contribute to content uniformity problems [8].

1) Non uniform distribution of the drug substance throughout the powder mixture or granulation.

2) Segregation of the powder mixture or granulation during the various manufacturing processes.

3) Tablet weight variation.

The uniform mixing of potent drugs is essential for assuring content uniformity of the final product. This is vital determining factor in case of drugs having narrow therapeutic window and a small change in drug content (in μ g or mg) altering the therapeutic range of drugs causing underdose or overdose. Both the situations are harmful for patients e.g. patient with congestive cardiac failure (CCF) taking digitoxin; under-dose causes therapeutic failure of drug and leads to death from CCF while overdose causes toxicity and chances of death due to development of arrhythmia.

A dry blending process for low dose drug is possible provided that the preblending and blending is carefully designed and process parameters are optimized [9]. The current article provides an overview on several formulation techniques for low dose drugs with their pros and cons in terms of homogeneity in the finished products.

General mixing problems and their solutions Segregation problem and its solution

Segregation refers to the separation of the coarse from fine material during the flow of a powder or the vibration of a bed of powder. It is the opposite effect to mixing [10] and can occur by several different mechanisms, depending on the particles physical characteristics and the handling method [11].

Segregation by sifting/percolation

Sifting or percolation is the movement of smaller particles through a matrix of larger ones [11]. It may be

produced by pouring a powder from one container to the next as is done by emptying the contents of blender into another hopper or into drums [12]. This is due to the particle size differences between individual components and interparticle motion.

In general larger the ratio of particle size, the greater the tendency for particles to segregate by sifting. If particles are stationary or moving with a uniform velocity, they are not essentially locked together, almost eliminating the tendency to segregate, even for high segregating mixtures. For sifting to occur, particles in the mixture must flow at different velocities [11].

Segregation by dusting/particle entrainment

Segregation may also take place during pouring of a powder; particularly of there is considerable free falling of the particles. In this case the fine particles become airborne and separate form the bulk of the powder [12]. This problem is particularly acute with pyramidal bins, as airborne fines that settle toward the walls eventually slide to the valleys (corners) of the bin [13].

Segregation by nature of flow of mixture

Segregation may also take place inside the blender when the powder bed does not exhibit mass flow characteristics, i.e. the powder does not flow from a hopper or mixer in the order in which it is situated in the container. In this case, the large particles move as the powder structure breaks down because of their larger mass, leaving the smaller structured particles behind [12].

Solution of segregation problems [10, 11, 13, 14]

 Selection of particular size fractions to get drug and excipients of the same narrow particle size range.

 Milling/size reduction of components to reduce the particle size range followed by sieving to remove fines or lumps.

 Controlled crystallization during production of the drug/excipients to give components of particular crystal shape or size range. 4) Selection of excipients with density similar to the active component (s).

 Granulation of the powder mix for even distribution of large number of different particles in each granule.

 Reduction of vibration or movement of powder mass after mixing.

 Use of filling machine hoppers designed so that powder residence time is minimized.

 Use of multi-operation equipments to minimize transfer of mix, e.g. a fluidized-bed drier or a high speed mixer or granulator for mixing and granulating.

Mixing by serial dilution method or ordered mixing.

10) Selection of correct equipment e.g., use of nauta mixer or ribbon blender rather than tumbling mixer. Traditional mass-flow bin can be replaced with mass-flow insert inside an existing bin in which insert consists of a hopper with in a hopper to provide uniform velocity profile in the bin that will minimize segregation.

11) Avoiding slopping surfaces in machinery.

12) Minimizing transfer steps, drop height, and controlling fluidization of powder.

Formulation techniques used for low dose unit dosage forms

Granulation techniques

Wet granulation technique

The drug is dissolved in water or another solvent, and blended with excipients including a binder, for example povidone, to form a wet mass containing 5-20% by weight of solution to total weight of granulation mix, which is then dried off in a separate step. The binder causes particles of excipient to lumps together, and as the mass dries these clumps ("granules") either contain or are coated with the drug. This is effective but cumbersome since the drying step requires special equipment, and generally involves high temperatures which may degrade labile drugs. Also, the use of the binder requires the further inclusion of a disintegrant such as sodium starch glycolate or starch to help the tablet, which is cohesive, to disperse in the stomach [15]. Desogestrel tablets (60 µg) were prepared by wet granulation using hydroxypropylcellulose as granulating agent in a Gral 10 granulator. Decomposition of desogestrel at 40 °C for two months at relative humidities of 10 and 95% was observed 0 and 1% respectively [15].

If the drug is unstable in water (like mestranol) then wet granulation process approach using organic solvents such as chloroform can be employed. Disadvantages of the process includes environmentally unsafe, considerable manufacturing expenses, in that appropriate solvent scrubbing and/or explosion proof equipment must be acquired at substantial capital expenditure.

Modified wet granulation techniques

This method utilizes an aqueous medium (water medium, with added water-miscible solvents such as isopropanol or ethanol if needed) which contains the active ingredient(s), a quantity of one or more surfactants sufficient to dissolve or suspend active ingredients uniformly throughout the medium and other manufacturing additives such as granulating-binding agents, pharmaceutical fillers, tabletting lubricants etc. This technique prevents migration of drugs through the carrier upon drying. Estradiol tablets (2 mg) were prepared by modified wet granulation using sodium lauryl sulfate, as surfactant and 1% povidone solution in water [16].

Modified wet granulation process was used for formulations of (2R)-(1 alpha, 5 alpha, 6 alpha)-N-[3-azabicyclo [3.1.0] hexyl-6-(aminomethyl)-yl] -2-hydroxy-2-cyclopentyl-2-phenyl acetamide hydrochloride. The process includes blending excipients, granulating blend with solution of drug in a rapid mixer granulator, drying and sizing of granules, blending granulate with other necessary excipients like lubricant and processing into a dosage form. Another process includes preparing a bed of excipients, wetting bed with solvent, granulating bed with solution of drug by spraying an atomized solution of the drug, drying and sizing of granules, blending granulate with other necessary excipients like lubricant and processing into a dosage form. [17].

Fluid bed granulation technique

Fluid bed granulation has been used to achieve

content uniformity of low dose (1 µg-10 mg) tablets. In this process, the micronised drug is blended as a powder with other excipients, then loaded into a fluid bed granulator and the powders are agglomerated by spraying on a solution of a binder; drying takes place concomitantly. The process does not require a separate drying step, but it does require the use of micronised drug and also incorporates a separate blending step prior to granulation. It also requires specialised equipment and precise optimization of the process parameters. This process overcomes the problem of mixing cohesive materials, which tends to occur during conventional granulation of microdose products and eliminates the adverse effects caused by differential solubility and hydrophobicity of the components.

Tablets containing micronized salicylic acid (which is hydrophobic and has a low aqueous solubility) were prepared using spray dried lactose as carrier material by interactive mixing in revolve cube mixer and granulating with polyvinylpyrrolidone. The content of tablets fell within \pm 15% of the mean and coefficient of variation was < 5% (99% confidence) for all batches [18].

Tablets of 2-methyl-2-[4-{[(4-methyl-2-[4-trifluoromethylphenyl]-thiazol-5-ylcarbonyl)amino] methyl} phenoxy]propionic acid (10 μ g) were prepared by fluid bed coating and preferred content uniformity % RSD = 2.5 (< 3%RSD) was achieved [19].

Carrier granulation technique

This functions by spraying a solution of binder such as povidone in water onto relatively large excipient particles such as hydrous lactose and then spraying small dry drug substance particles onto that, thus coating the excipient with drug particles which are stuck on by the binder. The quantity of solution used was 3.3-3.5% by weight of solution to total granulation mix. The method was applied to a formulation containing 4-5% drug by weight. This method also requires drying; the drug particle size needs to be very small, which often requires an extra milling step and the very fine drug powder may not flow at all well; and the formula still requires a disintegrant [20].

Spray drying using viscosity increasing excipients

This technique utilizes a viscous aqueous based spray solution (like starch, pre gelatinized starch, hydroxypropyl methylcellulose, methyl cellulose, povidone) to provide a uniform distribution of a small amount of drug in a large amount of granulation. After the water evaporates, drug is bound to the granulation reducing the potential for downstream segregation. The excipient providing viscosity to the aqueous solution act as "glue" and bind to the drug to the granulation after the water evaporates away. Preferably weight ratio of the viscosity increasing excipient to the pharmaceutical compound is from 12:1 to 60:1.

In this technique first paste of the viscosity enhancing excipient is prepared, drug is added to a portion of this paste to make a slurry (lumps may be present) and slurry is milled once or multiple times until it is a uniform suspension. Mill is then purged with the remaining paste to incorporate residual drug in the mill. Milled suspension and purge are then added to the spray solution tank for spraying onto the granulation using a fluid bed drier [21].

Dexamethaone tablets (0.25 mg) were prepared using starch as viscosity increasing excipient. The resulting dexamethasone tablets were uniform in potency and content uniformity testing gave an average of 101.2% claim with an RSD of 0.8% [21].

High shear granulation technique

In high shear mixer, powder is pinched between a moving and a static surface as in a comil or between two moving surfaces as in a pair of pressurized rolls. The speed of rotation is slow but the powder is subjected to very high shear that will breakdown most aggregates. It is commonly preceded by a convective or tumbler mixer to give a general bulk quality before the conditioning of the mixture on a microscale in the high shear mixer. In some cases the pressure exerted on the powder in the pinch zone is sufficient to consolidate it into a flake form. High shear mixers tend to have a limited throughput rate and are reserved for those mixtures requiring homogeneity on a microscale [22].

This process leads to the optimal mixing of the constituents of a pharmaceutical formulation, the process

is well-contained and the available modern equipment enables full in-process control [23].

Tablets containing 1 μ g or 0.1 μ g of 2-methyl-2-[4-{[(4-methyl-2-[4-trifluoromethyl phenyl]-thiazol-5-ylcarbonyl)amino]methyl}phenoxy]propionic acid were prepared by high shear granulation process. RSD of 1 μ g and 0.1 μ g tablets were observed at 2.1% and 1.5%, respectively [19].

Mefenamic acid (water insoluble) formulations were prepared by wet granulation using high shear mixing to study process parameters like amount of water added, impeller rotation speed, and kneading time. Result showed that increasing amount of water and kneading time led to an increase in particle diameter of granules and a decrease in mean pore diameter while increasing impellor speed led to a decrease in mean pore diameter but no effect on particle diameter [24].

Low shear granulation technique

Some micronised steroids such as desogestrel present in a low amount, the granulation process leads to a better content uniformity if the actual granulation step, i.e. wetting with binder liquid, while applying agitation, is conducted with substantially lower shear than normally applied in the current high-shear mixers. It was found that in a high shear mixer in a normal fashion, the content uniformity cannot be steered to RSD of below 3% and the demixing potential (DP) typically is 30-40%. When following the process of low shear granulation, an excellent DP of well below 10% and consequently favorable content uniformity was obtained.

This technique consists of a mixing step bringing into association the active substance and a suitable filler to form a mixture; a granulating step in which the mixture is granulated to form agglomerates or granules by wetting the mixture with a binder liquid, the wetting being conducted under agitation i.e. at low shear; post-mixing and compression for tableting or fill in capsules.

Desogestrel and ethinyl estradiol tablets were prepared by low shear granulation. DP for content desogestrel and content ethinyl estradiol was at observed 12% and 11%, respectively. Similarly desogestrel tablets (0.0075 mg) were prepared by low shear granulation technique. DP and tablet content uniformity in RSD were observed at 12% and 2.8%, respectively [23].

Novel foam granulation technique

In this technique foam of aqueous binder solution is prepared. Drug is dissolved in binder solution and wet granulations of drug while polymer with other necessary excipients is prepared using foamed aqueous binder solution in a high shear granulator. The granules are then compressed to form tablets. The foamed binders (like hypromellose 2910 USP, methyl cellulose USP) have a shaving cream which breaks quickly and disperses uniformly within the high-shear granulator. Formulation of propranolol HCI tablets (0.125, 0.25, 0.5, 1%) was achieved using hypromellose 2910 USP (1, 3 5, and 10% concentration) using foam granulation technique. Content uniformity testing of granulation and tablets showed a %RSD results range of 0.31 to 3.8% and 0.39 to 2.85% respectively [25].

Fluid bed granulation with jet pulverization

In this process formulations are produced by uniformly mixing drug combinations (e.g. one insulin sensitizer and an active drug (having a ratio of median size thereof to the median size of insulin sensitizer of 0.5 to 10) with additives or uniformly mixing after granulation and then compression molding. Mixing is performed using V-type mixer and granulation is performed using a high speed granulator, a fluid bed granulator-dryer. Desired ratio of median size of an active constituent with a large median size may be achieved by pulverizing it with an excipient like microcrystalline cellulose using jet mill, cutter mill or hammer mill.

Formulation of metformin hydrochloride and pioglitazone hydrochloride was prepared by mixing pioglitazone hydrochloride (median size 13 μ m) with microcrystalline cellulose into a mixer, pulverizing mixture in a jet mill pulverizer to give a pulverized product (median size 3.6 μ m) of a pioglitazone hydrochloride/ microcrystalline cellulose mixture. This pulverized product, metformin hydrochloride and microcrystalline cellulose

was casted into fluidized granulating dryer for granulation and then tableting. Coefficients of variation (%) of pioglitazone hydrochloride and metformin hydrochloride were observed at 0.6 and 0.5, respectively [26].

Compression techniques

Direct compression technique

The simplest way of manufacturing tablets is to blend all the ingredients as dry powders and tablet them. This is rarely successful for low-dose drugs; common problems being segregation of the powder blend during tabletting [27], fluidity, compressibility and maintenance of content uniformity. Proper selection of excipients in the formulation of low dose drugs could be employed to alleviate these problems in dosage forms prepared by direct compression technique.

Diazepam tablets (5 mg) were prepared by direct compression technique utilizing Emcompress[®] (Dicalcium phosphate dihydrate) as direct compressible vehicle. The Diazepam and Emcompress[®] at 1:1.5 ratio have imparted good tabletting properties and uniformity of mixing was satisfactory (S.D. of \pm 2.46%) due to the compatibility of particle size of diazepam and Emcompress[®] [28]. Fluoxetine tablets (7.5 mg and 15 mg) at low hardness (less than 5 kilopascal) were prepared by direct compression utilizing dicalcium phosphate dihydrate as diluents and microcrystalline cellulose as disintegrant at a ratio of 5:1 [29].

Experimental batches were prepared by mixing the active drug (0.07% w/w) with lactose anhydrous, Starch 1500[®] and microcrystalline cellulose and finally compressing after addition of other excipients. Content uniformity of final powder blend with lactose anhydrous, starch and microcrystalline cellulose were observed at 82.20 ± 4.61 , 90.65 ± 3.89 and 98.52 ± 3.98 , respectively. Mean drug content (%) \pm RSD tablets were observed at 92.43 ± 1.42 , 96.00 ± 1.25 and 99.59 ± 3.19 using lactose anhydrous, starch and microcrystalline cellulose, respectively [2].

Modified direct compression technique

Dose uniformity in formulations of highly potent drugs (50 μ g to 1000 μ g) may be achieved by dissolving

the drug in a solvent (like ethanol, methanol, acetone, tetrahydrofuran etc); distributing a solution of the active ingredient over a directly compressible tableting vehicle (like dicalcium phosphate dihydrate, compressible sucrose, lactose, mannitol, microcrystalline cellulose, modified starches) with subsequent evaporation of the solvent; adding lubricant and other excipients if desired, followed by tableting.

Formulation of (2S, 12bS)-1',3'-dimethylspiro-(1,3,4,6,7,12b-hexahydrobenzo[b]furo[2,3-a]quinolizin)-2, 4'-(5,'6'-dihydro-1'H-pyrimidine-2'(3'H)-one) tablets 50 μ g was achieved by this technique utilizing microcrystalline cellulose, as directly compressible excipient and anhydrous ethanol as solvent. Uniformity test showed satisfactory content uniformity (mean RSD=0.9781%) [30].

Dry blend compression of potent drugs with low solubility using directly compressible agglomerated excipients

Estradiol and a number of other low-dose potent drugs precipitate in a variety of polymorphs and/or crystal habits. The changes in the crystal structure on drying during wet granulation can affect the bioavailability of the drug [31]. This problem can be solved by utilizing dry blend compression using directly compressible agglomerated excipients.

The dry preparation makes use of excipients that have been prepared by agglomeration methods other than by spray drying (like granular mannitol, agglomerated maltodextrin, corn syrup solids, mixtures of these agents with added conventional direct compression excipients). Drug is located in crevices of the agglomerate which indicates a different mechanism of attachment. This technique is an important alternative to wet granulation, thus eliminating recrystallization and the issue of polymorphism and bioavailability.

Formulation of estradiol 2 mg tablets using agglomerated mannitol as directly compressible agglomerated excipient and formulation of medroxyprogesterone tablets using combination of agglomerated mannitol & maltodextrin was achieved [32].

Active layering and direct compression of sugar spheres

In this process layering of sugar spheres (250-355 μ m) is achieved by spraying drug contained in aqueous solution of binder followed by drying in a fluidized bed apparatus. The layered sugar spheres are then compressed into tablets after addition of lubricant. Layered sugar spheres show a much smoother surface which contributes to sphericity. The narrow distribution range of sugar sphere size, regular fluidization and solution spraying contribute towards uniformity of layering and this layering uniformity leads to a homogenous distribution of drug.

Formulation of acetaminophen (0.4% w/w) was prepared by active layering of sugar spheres using PEG 6000 as binder and compressing after addition of magnesium stearate as lubricant. Content uniformity data showed mean content value of 2.04 \pm 0.05 mg [33]. Similarly extended release tablets of ketoprofen with increased homogeneity were prepared by directly compressing dried micro granules obtained by coating neutral sugar spheres/quasispheres (after moistening with binder solution) with polymer material (for extended release like xanthan gum base, carbopol) by manual powdering in rotating coating pan (to increase the amount of polymer bound on sugar spheres and prevention of viscosity problems), drying and layering of this functionalized excipient by spraying solution containing drug and a binding agent [34].

Ordered mixing/Interactive mixing technique

Ordered mixing comes to yield the perfect mixture and may be obtained in a number of ways like mechanical means, adhesion, and coating. The major difference between the mechanical, the adhesional and coated ordered mixing is the degree of force holding the ingredients in each type of the ordered units together. Ordered mixing is not only beneficial in approaching a perfect mixture, but it minimizes the possibility of segregation of a mixture by holding the ingredient ratio constant via the intact ordered units [12]. Physicochemical properties of excipients significantly affect adsorption of small drug particles. Excipients with larger particle size, better flow ability and higher brasivity can help to break down agglomerates formed by very fine drug particles, adsorb individual drug particles onto the surface of large excipients, and improve homogeneity [35].

Fentanyl tablets (100 μ g, 200 μ g, and 400 μ g) were prepared by ordered mixing using adhesion method in which coarse mannitol particles were covered with fentanyl citrate by dry mixing to form an interactive mixture which then mixed with other ingredients and compressed into tablets. The average content was observed at 95-96% and uniformity of content (minimum-maximum) was observed at 88.2-101.4% [36].

Mixing of tetracycline (0.25% w/w) with spray dried lactose and fine grade of crystalline lactose was conducted. At this concentration both ordered and random mixing took place. Mixture quality was better (coefficient of variation = 1%) using a fine grade of crystalline lactose than with spray dried lactose (coefficient of variation = 4%) [37].

A 0.1% ordered mixture of cohesive salicylic acid and spray dried lactose excipient was stable when fluidized and no significant loss of salicylic acid occurred during fluid bed granulation. All batches of 100 and 350 mg tablets produced had a content coefficient of variation \leq 4.6%, a weight coefficient of variation \leq 1.5% [38]. Resemblance to an ideal ordered state in binary mixtures of sodium salicylate and mannitol was found with 0.15% drug proportion and the smallest particles [39].

Miscellaneous techniques

Low steroid dose dry pharmaceutical preparation by dry mixing

Low dose steroid drugs can be prepared by dry mixing of drugs with excipients having a demixing potential of less than 10% and a binding affinity of greater than 80% (like spray-dried polyalcohols, granulated alpha-lactose monohydrate, and mixtures of these) followed by adding further excipients for direct compression and compressing the admixture into tablets or filling in capsules. This process results into good properties with regard to robustness and ruggedness, while the resulting dry mixtures are very homogenous with regard to content uniformity even with very potent steroids.

A dry mix sample containing micronized ethinyl estradiol and spray dried lactose was made by mixing lactose with ethinyl estradiol for 2.5 mins. and good content uniformity (± 0.5%) was observed. Similarly ethinyl estradiol and 3-ketodesogestrel tablets, ethinyl estradiol and desogestrel tablets, desogestrel tablets, digoxin tablets were prepared using a dry mix process [40].

Dry blending with jet milling

Microparticles of active drug were blended with excipients and jet milling was used to deagglomerate microparticle aggregates formed during or subsequent to production of microparticles, by bombarding the feed particles with high velocity air or other gases. By proper selection of jet milling conditions, deagglomeration of microparticles were achieved without altering the size and morphology of particles. Typical jet mills used in process could include spiral jet mills, loop jet mills, fluidized bed jet mills, with or without internal air classifiers and blenders could be V-blenders, slant-cone blenders. dynamic continuous blenders, orbital screw blenders, planetary blenders, forberg blenders, horizontal double-arm blenders, horizontal high intensity mixers, vertical high intensity mixers, tumble blenders to attain satisfactory blend uniformity [41].

Homogeneous preformulations containing high concentrations of steroids, for producing low-dose solid and semi-solid pharmaceutical preparations

The technique of making the homogeneous steroid-containing preformulation includes the dissolving steroid(s) in a solvent (ethanol or a mixture of ethanol and water) to form a dispersant and dispersing an adjuvant consisting of adjuvant particles in the dispersant in a mass ratio of adjuvant to the steroid(s) of 1:1 to 1000:1 to form a suspension. Then, a spray-mist of the suspension is used so as to evaporate and remove the solvent from the suspension and thus to form a dried

particulate comprising a plurality of steroid-containing particles. The steroidal preformulations thus produced are mixed dry in a suitable mixture together with other direct-tablet adjuvants and then filled into hard gelatin capsules or in the form of an oily suspension in soft gelatin capsules, or tableted in the usual way. The tablets are made into lozenges or coated in aqueous or organic fashion, together with the usual, known adjuvants.

The process parameters to be controlled include particle size distribution of the active ingredient, solid concentration of the suspension, droplet size distribution in the spray mist, air inlet temperature, air outlet temperature, temperature for inflow of the suspension, spray pressure, nozzle size, drying air etc.

Preformulation of tablets containing 250 µg of sulfamate steroid was achieved using ethanol solvent, adding lactose monohydrate and then drying using drier with a dual-substance nozzle in the parallel flow process. The relative standard deviation was observed 1.28%. Similarly preformulation of desogestrel and ethinyl estradiol was done with satisfactory results [42].

Process for preparing solid unit dosage forms of ultra-low dose drugs using spray drying

In this technique active material is dissolved in a volatile solvent (methylene chloride, ethyl acetate, ethanol, methanol, fluorinated hydrocarbon (Freon)) and mixtures of these to form a very dilute solution of the active material. This solution is atomized and sprayed, in the form of a fine spray or mist of droplets of substantially uniform size, in a small amount, supplied over an extended period of time, onto fine, inert, excipient particles (insoluble in the solvent) that are undergoing continuous agitation (in an inclined rotating tumbler pan to ensure even distribution of the drug solution on the excipient particles) in a surrounding gaseous medium (to facilitate evaporation of the solvent) so that the droplets are substantially uniformly deposited on the excipient particles. The solvent is continuously and slowly evaporated into the surrounding gaseous medium and thereby a large number of very small solid particles of the active material become deposited uniformly on the excipient particles, without the occurrence of substantial agglomeration of the excipient particles or build-up of significant wetness in the excipient powder. Upon completion of the spraying and evaporation, the excipient particles having the very small amount of the active material deposited thereon are formed into individual solid unit dosage forms, such as tablets. Process parameters to be controlled include spraying rate of drug solution, total spraying time etc.

This technique is very useful to reduce particle size when milling cannot be used because drug particles are not monodispersed or in the case of heat labile drugs which on micronization are soften/melt and then agglomerated during micronization. Examples of known drugs advantageous for use in this technique include various prostaglandins, oxytocin and other peptides, vasopressin, vitamin B_{12} , VIP analogs, LHRH analogs etc [43].

Manufacturing a low dose pharmaceutical composition having uniform drug distribution and potency utilizing silicon dioxide

The process includes use of silicon dioxide (concentration 0.1 to 2%) for reducing the loss of active ingredients that adhere to the metal surfaces of equipment during the manufacturing process of a pharmaceutical composition or medicament. The addition of other glidant such as talcum or addition of a manual brushing step did not resolve the problem.

In this process silicon dioxide is blended with excipient, carrier or diluent in a high shear granulator to produce a blended mixture, and then active ingredient is added to the granulator and blended for an additional period of time to form an active blend. The active blend is transferred from the granulator to a blender like twin shell "V" or bin blender. Other excipients, lubricants, carriers or diluents to the active blend are added if required and blended for a suitable period of time to form a pharmaceutical composition having uniform distribution of the active ingredient and uniform potency. The resultant blended composition may then be processed further into a desired unit dosage form.

This process provides efficient mixing and a more uniform distribution of the active ingredient without significant degradation of the active ingredient. Loss of lasofoxifene due to adherence to metal surface of the blender can be minimized by means of silicon dioxide [44].

Spray-on liquid drug carrier

The model drug is dissolved in a non-volatile solvent, propylene carbonate and sprayed onto a compressible sugar at a loading of around 0.01% by weight of drug to total solid, to give a final unit dose of 35 μ g. The solvent, being non-volatile, remains in the blend. It is added at around 5% by weight of the total formulation. Lower ratios of solvent to solid resulted in decreased ability to disintegrate and dissolve. The result, somewhat sticky powder, showed some difficulties in automated encapsulation machines and would be likely to give significant problems in tabletting [45].

Formulation of rasagiline (1.6 mg) were prepared by wet granulation. The dry granulate was milled in an oscillating granulator to reduce particle size of drug less than 250 μ m. A lubricated blend was then prepared using a tumbler blender. The mixture was then pressed into tablets. Content uniformity of tablets ranged from 98.6 to 100.6% and RSD was lower than 2.0%. [46]. Similarly formulation of metformin/glibenclamide includes mixing step using tumbling mixer to achieve content uniformity [47].

Formulations of entecavir (0.01-10 mg active drug) were prepared by dissolving drug and adhesive (povidone, methyl cellulose, guar gum, gelatin etc) in a solvent (water or water having a acidic and basic pH to increase solubility of drug) at temperature 25-80 °C and spraying this solution onto a carrier (lactose, microcrystalline cellulose, dextrose, mannitol, sorbitol, calcium phosphate, etc.) in motion by mechanical means in fluid bed drier

or air stream agitation, drying, adding dried coated carrier with other necessary excipients to produce capsule or compressed tablets [48].

In spray drying technique, during handling of a mixture, demixing of active drug from carrier may occur due to difference in densities. This demixing can be prevented by adding an excipient having high specific surface area and a high electrostatic charge like silicon dioxide. This excipient is added to the carrier excipients before spraying the active drug solution. Formulations of warfarin sodium tablets (1, 2, 2.5, 3, 4, 5, 6, 7.5, 10 mg) were done by spray drying technique using silicon dioxide to prevent demixing of components with satisfactory content uniformity [49].

Micronized fentanyl citrate (1-10 μ m) have self aggregating properties which can be prevented by blending drug with hydrated dextrose to yield a matrix wherein drug particles are uniformly distributed over the surface of dextrose particles. The adsorption energy of the drug over excipient enables particle to break self aggregation. Oral transmucosal lozenzes of fentanyl citrate (200, 400, 1600 μ g) were prepared using dextrose to prevent aggregation of drug particles with content uniformity in average of 100.8, 100.7, 98.4%, respectively, with %RSD of less than 3% [50].

Formulations of $[R-(Z)]-\alpha$ -(methoxy-imino)- α -(1-azabicyclo [2,2,2]Oct-3-yl)acetonitrile monohydrochloride tablets (drug 5, 12.5, 25, 50, 75 µg per unit dose) were achieved by dissolving drug in water and adding to lactose monohydrate (directly compressible vehicle) in a high shear granulator, blending with magnesium stearate as lubricant and colloidal silica as glidant and compressing to tablet with satisfactory content uniformity [20].

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No.	Name of technique	Problem solved/advantages of techniques	Example of drug(s)	Major excipients used	References
	Wet granulation	Improvement of cohesiveness and compressibility of powders. Good distribution and uniform content of micronised or finely milled low dosage drugs. Reduction of a grate deal of dust and air borne contamination. Prevention of segregation of components	Desogestrel, Ethinyl estradiol	Calcium phosphate(di- and tribasic), Gelatin. Calcium sulfate dihydrate. Water soluble modified starches, Poly vinyl pyrrolidone, Sugars, Lactose	[15]
0	Modified wet granulation	Useful for drugs insoluble in water. Prevent migration of drugs through the carrier upon drying	Estradiol, Estrone Ethinyl estradiol, Methyl testosterone, Compound 2	Lactose 316, Nonoxyl, MCC, Croscarmelose sodium, Polysorbate 60, Polyoxyl 20 cetostearyl ester	[16,17]
ю.́	Fluid bed granulation	Rapid granulation and drying of a batch. Granulation prevents adhesion unit and constituent segregation occurring during compression. Eliminates the adverse effects caused by differential solubility and hydrophobicity of the components	Micronized salicylic acid, Compound 1	Poly vinyl pyrrolidone, Lactose monohydrate, MCC (Avicel PH 102)	[18]
4	Spray drying using viscosity increasing excipients	Prevention of segregation.	Dexamethasone	Starch, Povidone, Pre gelatinized starch, Hydroxypropylmethyl-cellulose, Methylcellulose	[21]
2	High shear granulation	Improvement in content uniformity. Full in process control	Compound 1	Sodium citrate, dehydrate, Croscamellose sodium, MCC	[19]
9	Low shear granulation	Prevention of segregation of components. Reduction of a great deal of dust and airborne contamination	Desogestrel, Ethinyl estradiol	PEG 400, Corn starch, HPC, Lactose 200M	[23]
8	Novel foam granulation Fluid bed granulation with jet pulverization	Improvement in content uniformity Improvement in content uniformity	Propranolol HCl Metformin hydrochloride, Pioglitazone hydrochloride	Hypromellose 2910, Methyl cellulose MCC	[25] [26]
0	Direct compression	Fluidity, compressibility and maintenance of content uniformity. Material handling is minimized	Diazepam, Fluoxetine	MCC, Microfine cellulose, Spray dried lactose, Compressible sugars, Sucrose-Dextran coprecipitate, Dicalcium phosphate dihydrate (Em compress)	[27,29]
10	Modified direct compression	Especially useful for formulating of drugs in which the unit dose is about 50 mg to 1000 mg. Unit operations are minimum	Compound x	Dicalcium phosphate dihydrate, Lactose, Compressible sucrose, MCC, Modified starches, Mannitol, Ethanol, Methanol, Acetone, Tetrahydrofuran	[30]
=	Method of dry blend compression of potent drugs with low solubility using directly compressible agglomerated excipients	Eliminate recrystallization and the issue of polymorphism and bioavailability observed during wet granulation	Estradiol	Granular mannitol, Agglomerated maltodextrin, Corn syrup solids	[16]

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No.	Name of technique	Problem solved/advantages of techniques	Example of drug(s)	Major excipients used	References
12	Active layering and direct compression of sugar	Increase reproducity in tablet weight and hardness. Prevention of segregation.	Acetamenophen, Ketoprofen	Sugar spheres, PEG 6000, Xanthan gum base, Carbopol	[33,34]
	spheres	Improvement in content uniformity			
13	Ordered mixing / interactive	Prevention of segregation.	Fentanyl citrate,	Coarse mannitol, PVP, Magnesium stearate,	[35,36]
	mixing	Promote excellent homogeneity in mixtures.	Sodium salicylate, Digitoxin	Silicified MCC	
		Improvement in content uniformity			
14	Low steroid dose dry	Minimize demixing.	Ethinyl estradiol,	Spray-dried polyalcohols, Spray-dried lactose,	[9,40]
	pharmaceutical preparation	Suitable for drugs which are sensitive to moisture	3-ketodesogestrel,	Cellactose(75% lactose and 25% cellulose),	
	by dry mixing	or are unable to withstand the elevated drying	DMP 543, Digoxin	Spray-dried mannitol, Sorbitol, Cellulose,	
		temperatures associated with wet-granulation methods		Xylitol, Dextrose, Fructose	
15	Dry blending with jet	Elimination of need of complicated wet	Alprazolam, Ziprasidone	Tween 80	[41]
	milling	deagglomeration process.			
		Increase stability of formulation by lowering			
		moisture and solvent levels in microparticles.			
		Improvement in content uniformity			
16	Homogeneous	Good stability of the active ingredient distribution in	Desogestrel, Ethinyl estradiol,	Lactose monohydrate, Ethanol	[42]
	preformulations containing	the pharmaceutical preparation.	Sulfamate steroid		
	high concentrations of	Nonhomogeneities and demixing or sizing effects			
	steroids, for producing	during the subsequent mixing process are avoided.			
	low-dose solid and	Applicable to thermally unstable steroids like sulfamates.			
	semi-solid pharmaceutical	Stable to demixing and nonhomogeneities.			
	preparations	No clumping and changes in activity of active ingredients			
17	Spray drying	Improvement in content uniformity.	Compound 1	Povidone, Lactose Monohydrate, MCC	[19,43]
		Applicable for heat labile drugs			
18	Manufacturing a low dose	Reduce the loss of active ingredients that adhere to	Lasofoxifene	Silicon Dioxide, Lactose, MCC, Croscarmellose	[44]
	pharmaceutical composition	the metal surfaces of equipment during the manufacturing		sodium.	
	having uniform drug				
	distribution and potency				
	utilizing silicon dioxide				

Abbreviations: Compound x = (2S, 12bS)-1, 3'-dimethylspiro-(1, 3, 4, 6, 7, 12b-hexahydrobenzo[b]furo[2, 3-a]quinolizin)-2, 4'-(5, 6'-dihydro-1'H-pyrimidine-2'(3'H)-one). Compound 1 = 2-methyl-2-[4-[[(4-methyl-2-1, -1)]] 2-[4-trifluoromethyl phenyl]-thiazol-5-ylcarbonyl)amino]methyl)phenoxy]propionic acid. Compound 2 = (2R)-(1 alpha, 5 alpha, 6 alpha)-N-[3-azabicyclo [3.1.0] hexyl-6-(aminomethyl)-yl] -2-hydroxy-2-cyclopentyl-2-phenyl acetamide hydrochloride. DMP 543 = 10,10-bis(2-fluoro-4-pyridinylmethyl)-9(10H)-anthracenone. MCC = Microcrystalline cellulose.

Conclusions

Mixing and formulation of low dose drugs are sophisticated work and involves lot of problems related to segregation, content uniformity and physical stability which can be controlled by right selection of material, method and machine. New and novel excipients have improved the science of low dose drug formulation. Advancement in processing parameters by optimizing various processes related parameters has put a stringent control on factors leading to segregation in powder mixtures. Processing and transfer steps are minimized to increase homogeneity in formulations. A summary of recent formulation techniques for low dose drugs have been provided in Table 3. Low dose drug formulations require micronisation to increase the number of particles of drugs which could be blended with other excipients to increase homogeneity in the formulation as well as final dosage form. The formulations are designed by various techniques to obtain granules, agglomerates or ordered mixtures so as to avoid segregation and handling issues.

References

- Indian Pharmacopoeia, Controller of Publications, New Delhi, 1996.
- [2] H. Ahmed, and N. Shah. Formulation of low dose medicines-theory and practice, Am. Pharm. Rev. 3: 1-5 (2000).
- [3] N. A. Orr, and E. A. Sallam. Content uniformity of potent drugs in tablets, J. Pharm. Pharmcol. 30: 741-747 (1978).
- [4] The United States Pharmacopeia-The National Formulary 30th ed, The United States Pharmacopeial Convention, Rockville, 2007, pp. 378-384, 630.
- [5] European Pharmacopoeia, The Directorate for the Quality of Medicines of the Council of Europe (EDQM), France, 2005, pp. 233-234, 3370-3373.
- [6] British Pharmacopoeia, The Stationary Office on behalf of the Medicines and Health Care Products Regulatory Agency (MHRA), London, 2008, pp. A 302-306.
- [7] T. Massa. Introduction to the PQRI blend uniformity working group manuscripts, PDA J. Pharm. Sci. Technol. 57: 59-74 (2003).
- [8] G. S. Banker, and N. R. Anderson. Tablets. In: L. Lachman, J. L. Kanig, and H. A. Lieberman (eds.), *The Theory and Practice of Industrial Pharmacy*, Varghese Publishing House, Bombay, 1991, p. 300.

- [9] L. S. Wu, J. G. Chen, and M. A. Hussain. Dry blending process scale-up for a very low dose drug candidate, AAPS *Pharm. Sci. Tech.* 1: 1-5 (2000).
- [10] H. J. Venables, and J. I. Wells. Powder mixing, *Drug Dev. Ind. Pharm.* 27: 599-612 (2001).
- [11] H. Purutyan, and J. W. Carson. Predicting, diagnosing, and solving mixture segregation problems, *Powder and Bulk Engineering*, 2006. Available from: http://www. powderbulk.com.
- R. J. Lantz, and J. B. Schwartz. Tablets. In: H. A. Lieberman,
 L. Lachman, and J. B. Schwartz (eds.), *Pharmaceutical Dosage Forms: Tablets*, Marcel Dekker, New York, 2005, pp. 15-20, 69.
- [13] K. Prescott. Powder Handling. In: M. Levin (ed.), *Pharma-ceutical Process Scale Up*, Marcel Dekker, New York, 2001, pp. 133-149.
- [14] A. Twitchell. Mixing. In: M. E. Aulton (ed.), *Pharmaceutics: The Science of Dosage Form Design*, Elsevier Science Ltd., Philadelphia, 2003, pp. 183,189-190.
- [15] D. Haan. Process of making dosage units by wet granulation, PCT Patent Application WO 96/09056, 1996.
- [16] F. C. Greaves, J. Swarbrick, M. W. Beansley, A. W. Suddith, and H. C. Caldwell. Method for preparing low dose pharmaceutical products, US Patent US 5976570, 1999.
- [17] K. V. Rao, P. J. R. Karatgi, and A. S. R. Murthy. Solid oral dosage forms of azabicyclo derivatives, PCT Patent Application WO 2006/003587 A2, 2006.
- [18] W. J. Thiel, L. T. Nguyen, and F. J. Sberna. Content uniformity of microdose tablets (dosage 1 mg-10 mg) produced by fluid bed granulation of interactive mixtures, *J. Pharm. Pharmacol.* 38: 335-343 (1986).120
- [19] P. Faulkner, R. Pan, and G. Provot. Low dose pharmaceutical products, PCT Patent Application WO 2005/097076 A2, 2005.
- [20] J. A. Napper, N. Mortimer, K. T. O'brien, S. J. Manek, R. Kumar, M. S. G. Clark, and J. M. Loudon. Process for preparing solid dosagr forms of very low-dose drugs, US Patent Application US 2003/0129246 A1, 2003.
- [21] P. W. Rice, and N. Mchardy. Dexamethasone containing formulations for oral administration as well the process for manufacturing required therefore, PCT Patent Application WO 2004/073685 A1, 2004.
- [22] N. Harnby. An engineering view of pharmaceutical powder mixing, *Pharm. Sci. Technol. Today* 3: 303-309 (2000).
- [23] V. Herman, and P. Janssen. Making dosage units using low shear granulation, European Patent No. 0955048, 1999.
- I. Ohno, S. Hasegawa, S. Yada, A. Kusai, K. Moribe, and K. Yamamoto. Importance of evaluating the consolidation of granules manufactured by high shear mixer, *Int. J. Pharm.* 338: 79-86 (2007).

- [25] P. Sheskey, C. Keary, U. Shrestha, and J. Becker. Use of a novel foam granulation technique to incorporate low drug loading into immediate-release tablet formulations, *Annual Meeting and Exposition of American Association of Pharmaceutical Scientists*, Baltimore, Maryland, Nov. 7-9, (2004).
- [26] M. Kolke, H. Koyama, and N. Hamaguchi. Solid preparation, US Patent Application US 2005/0287207 A1, 2005.
- [27] J. A. Napper, N. Mortimer, K. T. O'brien, S. J. Manek, R. Kumar, M. S. G. Clark, and J. M. Loudon. Process for preparing solid dosage forms of very low-dose drugs, PCT Patent Application WO 97/04750, 1997.
- [28] K. Abbulu, and V. Devi. Studies on applications and limitations of direct compression technology to low dose drugdiazepam, *The Pharma Review* (May-June): 79-86 (2004).
- [29] R. El-Rashidy, and B. Ronsen. Low dose fluoxetine tablet, US Patent US. 5830500, 1998.
- [30] A. V. Katdare. Method for tablet preparation, US Patent US. 4898736, 1990.
- [31] L. J. Lerner. Modified sequential oral contraceptive, US Patent US 3568828, 1971.
- [32] F. C. Greaves, J. Swarbrick, and M. W. Beansley. Method for dry blend compression of medicaments, US Patent US 5928668, 1999.
- [33] L. Martinez, P. Tchoreloff, M. Besnard, and G. Couarraze. Active layering and direct compression of sugar spheres: content uniformity in low-dosage tablets, *Pharm. Technol. Eur.* (October): 1-5 (2001).
- [34] P. Tchoreloff, B. Leclere, G. Benoist, and L. Bertocchi. Low dose tablets having a network of polymers, US Patent Application US 2008/0031946 A1, 2008.
- [35] W. Hong and Q. Yong. Adsorption of small drug particles at the surface of large excipients, *Pharm. Technol. Eur.* (January), 2006. Available from: http://www.ptemag.com/ pharmtecheurope/Analytical/Adsorption-of-small-drug-particles-at-the-surface-/ArticleStandard/Article/detail/285078.
- [36] S. Bredenberg, M. Duberg, B. Lennernäs, H. Lennernäs, A. Pettersson, M. Westerberg, and C. Nyström. *In vitro* and *in vivo* evaluation of a new sublingual tablet system for rapid oromucosal absorption using fentanyl citrate as the active substance, *Eur. J. Pharm. Sci.* 20: 327-334 (2003).
- [37] M. C. R. Johnson. Powder mixing in direct compression formulation by ordered and random processes, *J. Pharm. Pharmacol.* 31: 273-276 (1979).

- [38] W. J. Thiel, and L. T. Nguyen. Fluidized bed granulation of an ordered powder mixture, *J. Pharm. Pharmacol.* 34: 692-699 (1982).
- [39] S. Sundell-Bredenberg, and C. Nystrom. The possibility of achieving an interactive mixture with high dose homogeneity containing an extremely low proportion of a micronised drug, *Eur. J. Pharm. Sci.* 12: 285-295 (2001).
- [40] D. H. Pieter, and M. J. Deurloo. Low dose dry pharmaceutical preparation, European Patent EU 0503521, 1992.
- [41] D. A. Chickering, S. Reese, R. S. Narasimha, J. A. Straub, H. Bernstein, D. Altreuter, and E. K. Huang. Methods for making pharmaceutical formulations comprising deagglomerated microparticles, US Patent Application US 2006/00993678 A1, 2006.
- [42] M. Dittgen, D. Grawe, P. Hoesel, P. Moellmann, C. Timpe, and K. Matthey. Homogeneous preformulations containing high concentrations of steroids, for producing low-dose solid and semi-solid pharmaceutical preparations, US Patent US 6290931, 2001.
- [43] S. H. Yalkowsky. Process for preparing solid unit dosage forms of ultra-low dose drugs, US Patent US 4489026, 1984.
- [44] D. S. Gierer. Method for manufacturing a low dose pharmaceutical composition having uniform drug distribution and potency, PCT Patent Application WO 02/087546 A2, 2002.
- [45] T. C. Dahl, and G. Burke. Feasibility of manufacturing a solid dosage form using a liquid nonvolatile drug carrier: a physico-chemical characterization, *Drug Dev. Ind. Pharm.* 16: 1881-1891 (1990).
- [46] T. B. Peskin. Rasagiline formulations of improved content uniformity, US Patent Application US 2006/0188581 A1, 2006.
- [47] Y. Bonhomme, G. Nicholson, G. Cave, and S. J. Nicholson. Solid oral dosage forms comprising a combination of metformin and glibenclamide, US Patent US 6303146, 2001.
- [48] R. J. Colonno, O. Sprockel, A. Harianawala, D. Desai, and M. G. Fakes. Low dose entecavir formulation and use, US Patent US 6627224, 2003.
- [49] A. Franc, B. Zaludek, R. Gonee, M. Maleeek, H. Tkadleekova, and A. Petrovieova. Method of producing dosage units of a solid drug form containing warfarin sodium salt as active component, US Patent Application US 2007/0026077 A1, 2007.
- [50] C. N. Jobdevairakkam, and B. Selvaraj. Composition of fentanyl citrate oral solid transmucosal dosage form, excipient and binding material thereof and methods of making, PCT Patent Application WO 2007/058923 A2, 2007.